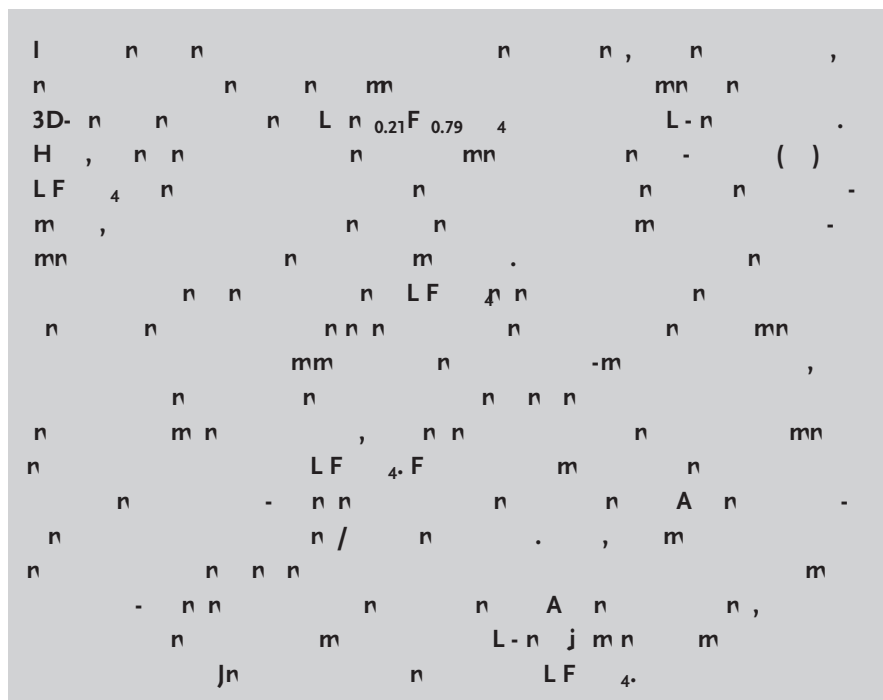


Li-Ion Battery

Jiangtao Hu, Wen Li, Yandong Duan, Suihan Cui, Xiaohe Song, Yidong Liu, Jiaxin Zheng, Yuan Lin,* and Feng Pan*



1. Introduction

This work reports on the synthesis and electrochemical performance of LiMn_{0.21}Fe_{0.79}PO₄ (LIB) as a cathode material for Li-ion batteries. The LIB material was synthesized by a solid-state reaction method. The electrochemical performance of the LIB material was evaluated by cyclic voltammetry (CV) and galvanostatic charge/discharge (GCD) tests. The results show that the LIB material exhibits a high capacity of 108.45 Ah g⁻¹ at 100 °C and a high cycle life of 150.21 Ah g⁻¹ at 100 °C. The LIB material also shows good rate performance and excellent low-temperature performance.

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a ead X-a ic c a%, Li e%. a ed the d a ic f the Li c i% a di e% a% i% i- a LiFePO₄ a %e.^[10] The e e% d ha e he f i igh% i % the Li i % ca a% / dei % ca a% i e% i% LiFePO₄ a %e, b % the e% d % % the i % ic eec% che ica e % f i ge LiFePO₄ a c % i % ac i g.

C c ic % e% (CV) i a e i% e a d i a ide ed %ch i e f %e i e %ga% f eec% che ica i e%. Gi e %a% Ga a %% I % i% % Ti%a% Tech i e (GITT) a d Eec% che ica I eda ce S ec% c (EIS) a e a icabe % id- % eac% % a d ca % be a icabe % LiFePO₄ d e % i% a% di cha ge a%,^[11] a d PITT ea e e %a ea%e % c e, CV e% d d be a ea ia% e% d %d %e i e% f eec% che ica e f a ce f LiFePO₄. M % f %die i g %i e% d a e i % i g a d a %ge f %e e a- %^[11] $I = 2.69 \times 10^5 n^2 A(D_{Li})^{1/2} v^{1/2} \Delta c_0$ (I : ea c e %n: %e eec- % ic be a %i a% g i %e eac% ; A: %e eec% de a ea i e ed i % ; D_{Li}: Li-i diff i c ef cie %v: ca eed; C₀: c ce %a% a ia% bef e a d a f% %e eac%) % e a a% diff i c ef cie %^[2] eec% che ica i d^[13] a d ea e ca aci% ce c %ab %.^[14] We ha e e ed CV %g % b% i %e ea%e a a e% % de - %a% %e ea h LiFePO₄ ha %ahigh a% ef - a ce i a e eec% %.^[15] He %dge' g^[16] de i e a e e% d f %e di ec%e %ac% f i e% d a% f e e i e % CV b e ica i a%, ba ed %e B % V e (BV) f c% a d %e Fic' diff i a. F %e - e, %e i % d ce %e a e%ac Ma c H h Chid e (MHC) %e % %e %d f face-b d ed c e i CV c e a d ge% %e a %f %e e ga i a% e eg a d %e a e% a a e% Tafe % H e e, a % a CV da% i e i i% a% e a ec ec% d b % % %ic eec% de f ba% %e e c% %e e a cha ac% i % f %e i g eec% de.^[17] Th gh %e e di g a e ef a d ci e % ca ea i g f %e ac%a %i a% f %e ba% , %ge%acc a% a d a %e e i f a% f %e CV % % fa i ge a c % da be ff da e % i % e % a di % %f %e ac%a %i a% .

I %i , e de e ed a e e% d % f %a% i i ge- a %e (SP) eec% de f LiFePO₄, i hich LiFePO₄ a a %e c d be f ca% ed a d di %ab %d % c - %c% i% %e c d c%e e% f cab a %be (CNT) (c d c%e cab e%). The ha e %CV ea f %e SP eec% de a b% i ed % %d %e i %a ic eec% che ica e % f LiFePO₄ a c % . We a de e ed a e SP- de f LiFePO₄ i% %e e % %a% i% ca de c i be %e ea% hi be %ee eac% a% a d %ge ec i e b i g da% f %e e i e % % %a- ca aci% (a i ed a %ge % % f cha ge (SOC)) c e f LiFePO₄ % e ace %e Ne %e a% . B i g %i SP- de % % %e e e i e % CV c e f SP eec% de f LiFePO₄, e a ge% %e diff i c ef cie %a d face eac% c ef cie % f LiFePO₄ a c % i %e a e a d ga ic eec% % a% diffe e % % e a% e. The e % a % %e h %a% %e i %a ic Li-i diff i c ef cie % f LiFePO₄ a e ea %e a e i a% a d ga ic eec% %, b % %e i % facia a% c % %a a% eec% %i e de highe %a %a% i g a ic eec% %, hich ca be %e deci i e fac% f %e

e ce e %a% ef a ce i a e eec% % f LiFePO₄. B i e %ga% g %e % e a% e effec% f i % facia a% c - % % %e i igh% f e- e %a fac% a d %e ac% e e e g f %e i % facia eac% e a% ca be de %d f %e % %e, hich a e e a% d i% de a% / a% ce a d id i di % face % c% e f LiFePO₄, e ec% e .

2. n D n

2.1. n E

Figure 1a h %e c % % c% e f %e %e i ed LiFePO₄@C d c%, hich e hibi% a i ge- ha e i i e- e % c% e i% P a ace g (JCPDS NO. 81-1173). Rei%e d e e e % f X- a diff ac% (XRD) da% i c d c% d % ide - %f %e a% %e c % %a d c %a% %e e a e i i% ha e (Fig e S1, S %g I f a%). The ca i ge ec- % ic c (SEM) ic% e f LiFePO₄@C e e h i Fig e 1b, a d %e ea a %e i e f LiFePO₄ i ab %40 .

T e a e %e SP LiFePO₄ eec% de, e e fac% , ch a %e % e- ca e f %e %a ic di e i f a a %e i a d %e %ic e f %e eec% de %achie e SP e- f a ce, e e %i e %ga% d. We de ed %a% %e %i eec% de i% e ha CV ea h e eec% de a% - ia ha e fec% a %e di e i i% g %a ic %e a SP eec% de. D i g e e i e % e did CV % % i b % a e a d ga ic eec% % i g %a% i eec- % de i% %e a e de diffe e % %a ic %e (Fig e S2 a d S3, S %g I f a%). Ob i , %e CV ea cha ge ha e i% %e ge %a ic %e, a d %e ha f id% ea e ai c % %af% 50 i %a ic. The e d be % fagg e a% i% h % %a ic %e, a h i Fig e S4 a d S5 f %e S %g I f a%. We a did E eg Di e i e S ec% c (EDS) ea e - e % f a% ia i% 70 a d 5 i %a ic %e, a h i Fig e S6 f %e S %g I f a%, hich did %h di %g i hed diffe e ce fee e %di %ab % de % %e e % i i% The e %e %e 70 i %a ic a% ia f f %e % % hich d be di e ed e gh % f SP eec% de. The % i ed a % f c d c% e cab i %e cea% c d c%e e% % ed ce %e e i % ce f eec% de a d % e a a% LiFePO₄ a c % a i ge- a %e e bedded i c d c%e cab e%. I de % % %e %ic e f eec% de, e d ed %e (af% %a ic f 70 i) a % i% c % i% %e %a% i (a ca e, ab %100 200 %ic, Fig e S7, S - %g I f a%) a d i% a %ic (ic e% i e, ab %7 μ, Fig e S8 f %e S %g I f a% a d Fig e 1c) eec% de, e ec% e. The CV e f a ce f %a% i eec% de f ed i% %e dee - di e ed (af% %a ic f 70 i) e %ha e % % ch % e f eec% de c d be ca ed a SP eec% de i %i %d. He ce, % e a e %e SP eec% de, e h d % e ca e f % e fac% : % f a %i eec% de (e i i a% %e c ce %a% a i a% f eec% de) a d % %e g %a d % ef di e i g % dec ea e agg e a% .

Fig e S7 a d S8 a f %e S %g I f a% h %e di - %ab % f %e e a ed SP eec% de a d %ic eec% de d ed

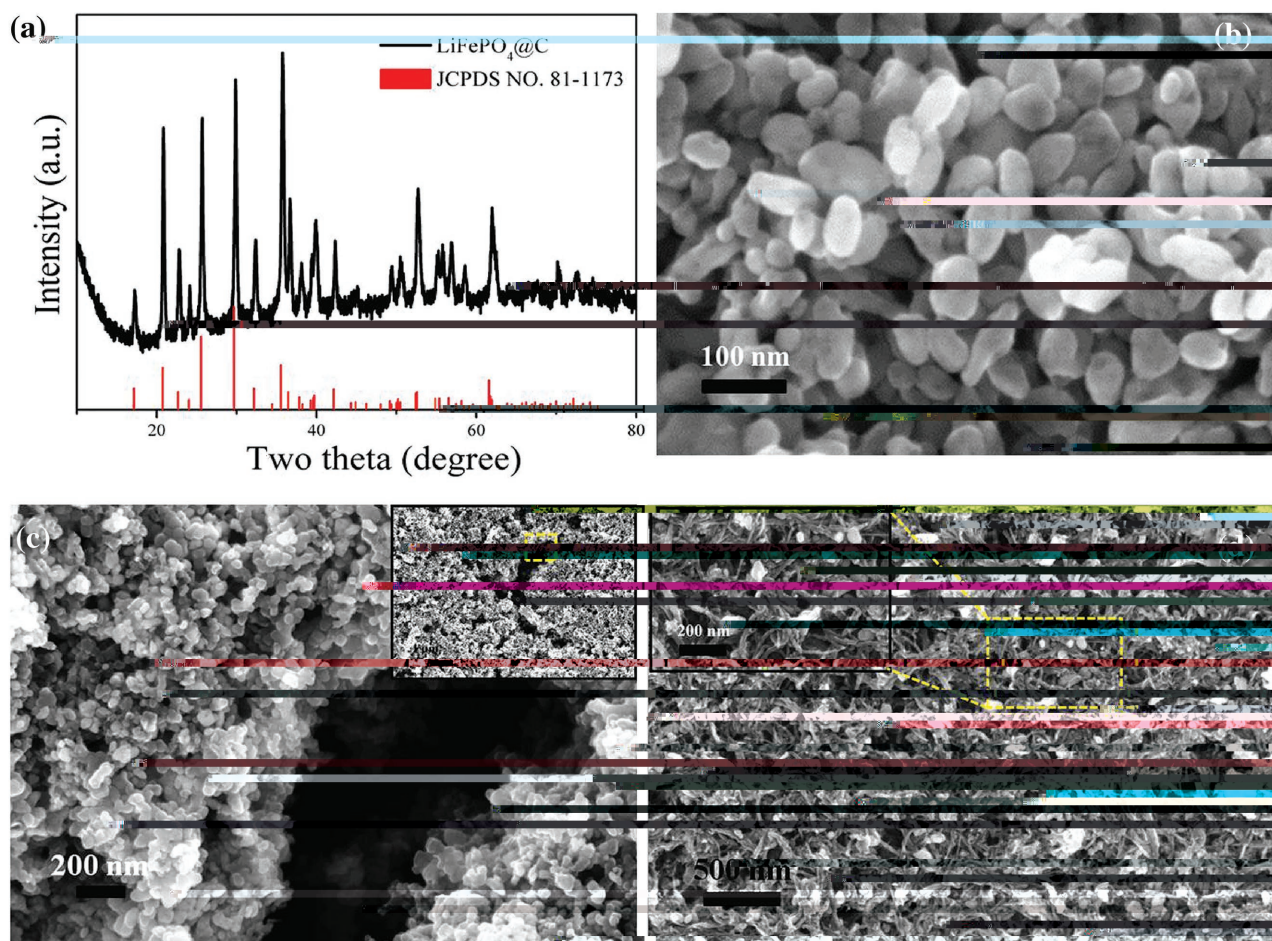


Figure 1. a,b) XRD and SEM data of $\text{LiFePO}_4@\text{C}$. c) The 3D confocal images of thick electrode dropped on quartz monitor crystals. d) The spatial structure of SP electrode using CNT.

a) i% c % b 3D c f ca, a d %e heigh% f %e %i a d %ic eec% de a e a cae a d ic e% i e, e ec% e . Fig e 1c a d Fig e S7 ba d S9 (S % g I f a%) h %e a%a % c% e a d h i ca a f %e % i d f eec% de . Ob i , %e SP eec% de h c % c% d a - a %e (LiFePO_4 a c % i% ea i e f ab %40) e bedded i c d c% e ca b a a %e (a ab %40) % a e a e% i% e (10 20) a d ac (100 500), h i ch a e ad % each LiFePO_4 a c % c e % c % c % i% c d c% e e% f e d b c d c% e ca b a a %e a d eec% % f eec% i ca d Li- i c d c% f cie %, e ec% e . Th , %e SP eec% de c d i i e %e c ce %a% a i a% , eec% che i ca a i a% , a d %e i % a i % f e e ce % b e % f % % g %e i % i ce e c% che i ca e % f LiFePO_4 i ge a %e . Fig e S10 f %e S % g I f a% d i a %e heigh% d i %b % f eec% de a % i a c a% g a % i% c % b % e . B c %a %e %ic eec% de h a c e c % c% d a a - %e- e% i% e e a d ac , h i ch d e a i ge e a% c ce %a% a i a% a g %e %ic - di ec% f a eec% de d i g %e cha g i g d i cha g i g ce f LIB .

Si i a , e cha ged %e ca b bac % CNT i% %e %a ic % e f 70 i . I% ca be ee %a %e LiFePO_4

a a %e c d be ca % ed a d di %b %d %c %c% i% %e CNT- e% e e , a h i Fig e 1d. Addi% a , e ad %d %e % f LiFePO_4 a c % a d ca b bac % ea i e a ab % i ge- a % e eec% de . N % %a% he i e i ca e d %e a% f ca b bac % LiFePO_4 a c - % % e %a 1:1 i eigh% %e CV c e e e ed e ca aci% ce i f a% (Fig e S11, S % g I f a%) . A % i e d a % f c d c% e ca b bac i % e d ce %e e i % ce b e %e %e a %e a d %e e i ece, b %a ca e a a% %e LiFePO_4 a %e a d ed ce %e i % a %e i c eec% i c %a %i i% . Th , c - d c% e ca b a a %e a ce a% %e c d c% e e% , h i ch a i i a e a CNT, % f ca % a d di %b % LiFePO_4 a a %e % c %c% i% %e c d c% e e% , e % g i %a %b % %e f SP eec% de e h i b i %e ha e % CV c e .

2.2. E m

CV % % eec d c% d %e e% i d f %ic (a c i ce) a d SP eec% de i diffe %e eec% % c i c - % ce . A %e ad fa c% e a % i a a %e ac% %e a e ,

Figure 2a,b. Obi, c, aed i% the %ic eec% de a d
a c i ce, i%ca be be ed %a%the a dic ea f SP
eec% de a e e ha , %e ha f id% f SP eec% de i ch
a e, a d %e g adie %ff e' i i g edge i a highe.
N % %a%ca% de ea f SP eec% de h %e a e i d f
ef a ce a h i Fig e S12 a S13 f %e S %g
I f a% . I %e %g , e % cha ge/di cha ge % %a-
ca aci% % %f %e % eec% de i a e a d ga iceec-
% % a%0.2 C (1 C = 170 A g⁻¹), e ec%e , a d f d %a%
%e di cha ge c e f SP eec% de a d %ic eec% de e e
a %c i cide %a b %e ec% % (Fig e 2c). S a e %
i a ed: h d %e cha ge/di cha ge % %a-ca aci% c e
f SP a d %ic eec% de ee i% %e a e i% %e i i a
cha ge/di cha ge a% (ab %80% ca aci% a% %a e
%ge), b %e CV da% h ch a big diffe e ce be%ee SP
a d %ic eec% de , cha %ef id%a%af a% f CV
f SP eec% de a d %ic eec% de 0.015 a d 0.071 Vi a e ,
a d 0.032 a d 0.078 Vi ga iceec% % , e ec%e ?

Ge e a , % e e a e % i d f CV i a % de: BV
de a d MHC de (e e % E e i e % Sec %). The
CV c e f c i c e i g a i c e e c % % c a b e % d e
b e i c a i a % b a e d BV de (Fig e 2d), i di-
c a % g % e BV e a % c a b e a i e d % % i c e e c % de f
LiFePO₄. The e a d % d % e a d % a f e c e f c i e % a d
diff i c e f c i e % f BV de a d e a c % c % % f
MHC, h i c h de % i e % e h a e f CV, % % e CV c e
f SP e e c % de i % e % e e c % % . S i i g , e e
h e e a d % d % e e f a c % % % e i i % , i % i -
i b e % % % e e e i e % c e e e (Fig e S14, S -
% g I f a %). Ob i , % e BV a d MHC diff i
de i i i b e % de c i b e % e SP e e c % de f LiFePO₄
a c % .
F % e i i e d e e c % c h e i c a e a c % , e a
c i d e d % e a % a f e c e a d i % f a c e c h a g e
% a f e c e . I e i CV a a i , % e % c -
e c % e d a % a f e c e a e a d i g i
h a f i i % a e h i e % e i % f a c e c h a g e % a f e c e

The decomposition of LiFePO_4 at 500°C in air was studied by thermogravimetric analysis (TGA) and differential scanning calorimetry (DSC). The TGA curve shows a weight loss of approximately 15% between 400°C and 500°C , which is attributed to the decomposition of LiFePO_4 into Li_2O , Fe_2O_3 , and P_2O_5 . The DSC curve shows an endothermic peak at 450°C , corresponding to the decomposition reaction. The decomposition reaction is given by:

$$4\text{LiFePO}_4 \rightarrow 2\text{Li}_2\text{O} + 2\text{Fe}_2\text{O}_3 + \text{P}_2\text{O}_5$$

The decomposition of LiFePO_4 in air at 500°C was also studied by X-ray diffraction (XRD). The XRD pattern shows the formation of Li_2O , Fe_2O_3 , and P_2O_5 phases, confirming the decomposition reaction. The decomposition of LiFePO_4 in air at 500°C was also studied by scanning electron microscopy (SEM). The SEM image shows the formation of a porous structure, which is characteristic of the decomposition product.

Ba ed %he ab e a i, e c %c%a e SP- de
 i %hi hich i c ed f diff i ce a di %-
 face cha ge %a fe ce . D i g %he ida% ce f
 CV ca i g, %he i % a Li-i i %hi LiFePO₄ (LFP) a -
 %e begi % ead % %he diff i ce a % e %he
 Fic ' diff i a (E a % (1), %he ig i ca% a d i %
 a e de ic %d i Tab e 2)

$$\frac{\partial C(x,t)}{\partial t} = \frac{D_{\text{li}}}{x^2} \frac{\partial}{\partial x} \left(x^2 \frac{\partial C(x,t)}{\partial x} \right) \quad (1)$$

A f %e i % face e ec% e cha ge ce de c ibed
 i %e B %e V e e a% (E a% (2)), %e %e eac-
 % a% i e a % %e ida% a% c % %(k_0) %
 ied b %e ed c% %c ce %a% ($C(R, t)$) a d %e
 i %e ed c% a% c % %(k_{Re}) % ied b %e
 ida% %c ce %a% ($C'(R, t)$), hich a i% %
 SP- de

$$i = \text{FA} \left(k_o C(R, t) - k_{\text{Re}} C'(R, t) \right) \quad (2)$$

Here, the high density of the LiFePO_4 SP electrode compared to the bare NE electrode (E_{onset} (3) and (4)). A large amount of NE can be electrodeposited on the LiFePO_4 surface, which could be attributed to the high surface area of the LiFePO_4 electrodeposited on the NE electrode, which could be attributed to the high surface area of the LiFePO_4 electrodeposited on the NE electrode.

$$k_{\text{Re}} = k^0 \exp \left\{ -\alpha^{\circ} \frac{F}{RT} [E - E^0] \right\} \quad (3)$$

$$k_o = k^0 \exp \left\{ (1-\alpha) \frac{F}{RT} [E - E^0] \right\} \quad (4)$$

The $\text{e}^{\%}$ f SP de i $\text{e}^{\%}$ eci e ea% hi be% ee eac% a% a d $\text{e}^{\%}$ ge (E a% (5)) hi ch i g % b i g $\text{e}^{\%}$ ea % $\text{e}^{\%}$ -ca aci% (a i ed a $\text{e}^{\%}$ ge-SOC) c e f LiFePO_4 (Fig e S15 bac i e, S $\text{e}^{\%}$ g l f a- %) % e ace $\text{e}^{\%}$ Ne $\text{e}^{\%}$ a% , beca e $\text{e}^{\%}$ Ne $\text{e}^{\%}$ a- % ca % de c i be % $\text{e}^{\%}$ -SOC c e f $\text{e}^{\%}$ LiFePO_4 a c % SP e c % de

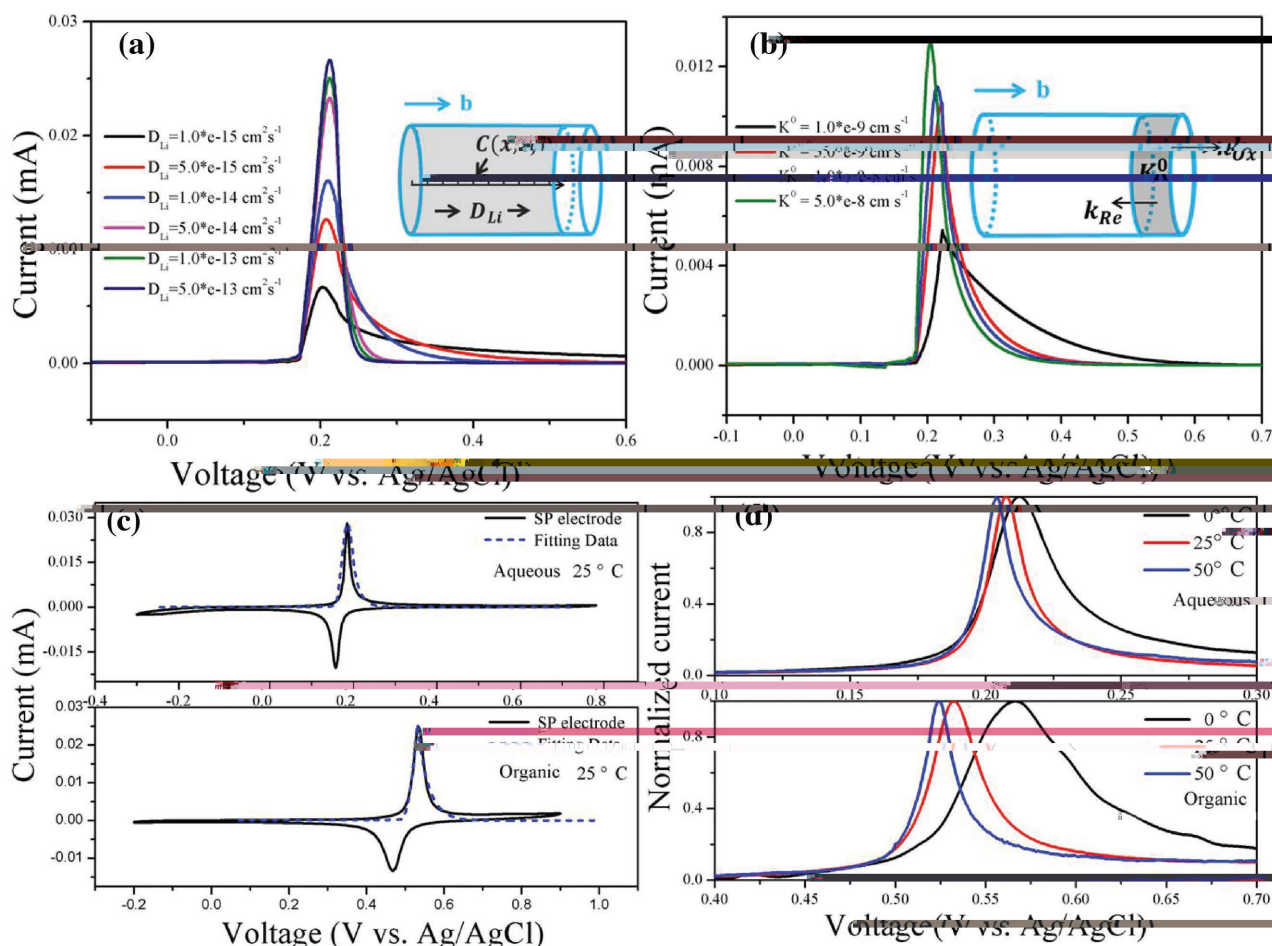
$$k_{Re} \propto -f(E(soc)), \quad {}^\infty k_{Ox} \propto {}^\circ f(E(soc)) \quad (5)$$

$$K_{eq} = \frac{k_{Ox}}{k_{Rp}} = \frac{(1 - SOC)}{SOC} \quad (6)$$

B i g h e a c a d c e (SOC) f a c a d c e a e i e e a h i (E a % (6)) a d d i g E a % (5) a d (6) i % E a % (2), e c a g e e a h i b e e e g e a d c e % e % i - a % CV d a % f S P e e c % d e . (The d e i d i f a % a b % SP- d e a d e c i b e d i % E e i e % S e c % .) Figure 3a h h D_{Li} a f f e % h a e f a C V c e , c h a % i - a d C V c e i % e d a a e % ($K^0 = 1 \times 10^{-8} \text{ c }^{-1}$, $\alpha = 0.5$) a d % i g D_{Li} (f $1 \times 10^{-15} \% 5 \times 10^{-14} \text{ c }^{-2} \text{ }^{-1}$). We c a e e % h e D_{Li} i c e a e , % a d i a f f a i g e d g f % C V c e i a i c e a e d a d % a i i g i a i h e d , b % h a f i d % i a i c e % c % % S i i a , % e d f % c h a g e f C V h a e i % K^0 (f $1 \times 10^{-9} \% 5 \times 10^{-8} \text{ c }^{-1}$) a h i Fig e 3b h e % a a e % e e d (D_{Li}= $1 \times 10^{-14} \text{ c }^{-2} \text{ }^{-1}$, $\alpha = 0.5$), i h i c h % g a d i e % f i i g e d i i c e a e d b i h e e a h a f i d % i d i i h e d i % a e f i c e a i g

1. The simulation data of SP electrode at different temperatures in different electrolytes.

Parameters		Aqueous [°C]			Organic [°C]		
		0	25	50	0	25	50
D_{Li} (cm ² s ⁻¹)	Charge	$>1.8 \times 10^{-14}$	$>2.8 \times 10^{-14}$	$>1.4 \times 10^{-14}$	$>1.5 \times 10^{-14}$	$>3.0 \times 10^{-14}$	$>3.0 \times 10^{-14}$
	Discharge	$>1.0 \times 10^{-14}$	$>2.0 \times 10^{-14}$	$>2.8 \times 10^{-14}$	$>1.5 \times 10^{-14}$	$>3.0 \times 10^{-14}$	$>3.1 \times 10^{-14}$
K^0 (cm s ⁻¹)	Charge	4.3×10^{-9}	2.0×10^{-8}	7.0×10^{-8}	8.0×10^{-10}	3.0×10^{-9}	9.0×10^{-9}
	Discharge	4.0×10^{-9}	1.8×10^{-8}	6.0×10^{-8}	7.0×10^{-10}	3.0×10^{-9}	9.0×10^{-9}



F 3. a) The variation tendency of CV curves with the increase of diffusion coefficient by SP-model. b) The variation tendency of CV curves with the increase of interfacial rate constant by SP-model. c) The CV curves of SP electrode and thick electrode in aqueous and organic electrolyte at 25 °C with the current density of 1 mV s^{-1} , the dotted lines are the simulation curves by the SP-model. d) The CV curves of SP electrode at different temperature in aqueous and organic electrolyte with the current density of 1 mV s^{-1} .

K^0 . Mei %%, % gh SP- de (he e de)
(Fig e S16, S % g I f a %) b ad % g % e ea % d
aa e % , % e i a % d CV c e ca be % d e fec % e
i % % e e i e % c c i c % g a f % e e a e d
LiFePO₄ SP e e c % d e (Fig e 3c) f % e % % e , a d % e
b % i e d aa e % e e d e i c % d i Table 1. (The e cha g e c -
e % d e i % a e e e d i Tab e S2, S % g I f a % .)
I d e % e i f e e i e % e % d a d SP d e , e
ha e d e a c e a % e e i e % i g CNT a % e c d c -
% e e % , % e e e i e % d a % a d a e % a e h i
Fig e S17 a d Tab e S3 f % e S % g I f a % , a d % e
i a % e % e % a % e a e i % % e i g c a b
b a c a % e c d c % e e % . M e e , e h a e a b i % a
a % d e . The i % i i % a % d i e c % i b f LiFePO₄,
a d e c a c a % d % e e g % a b % e (010) face b Sche e e a -
% (27.3). C b i g i % % e a b e i f a % , e % a
i a % f % e SP e e c % d e d e d i f f e e % % e a % e i %
d i f f e e % e c % % (a e a d g a i c). The i a % c e
a d d a % a e h i Fig e S18 a d Tab e S4 f % e S % g
I f a % . The a g i % d e f d i f f i c e f c i e % d i % f a c i a
a % c % % a e a % e a e .

2.4. The Effect of Temperature on the Electrochemical Performance of LiFePO₄

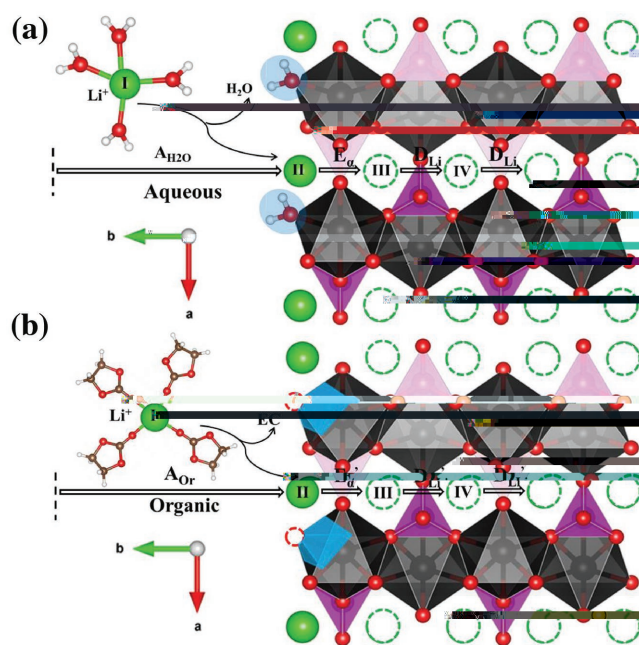
T f % e % d % e a % e e f f e c % , e d i d % e CV % % i d i f -
f e e % % e a % e (0, 25, a d 50 °C) a % a e a d g a i c
e e c % % , e e c % e , % e e % e e e c % c h e i c a c h a c -
% i % f LiFePO₄ (Fig e 3d). I d e % c a e % e cha g e
% e d f CV c e i d i f f e e % % e a % e c e i e % , e
a i e d i % d i d i g % e a i a e f e a c h CV d a %
I % c a b e b e d % a % % e g a d i e % f i i g e d g e i i %
% e i c e a i g % e a % e a d % e h a f i d % b e c e a -
e , b % % e e a e a % b e i % e d i f f e e c e i % e % a i g
a % d e d i f f e e % % e a % e . I d e % c a i f % i h e
e , e e a e d e e c % c h e i c a c e (Fig e S19
a d S20, S % g I f a %) a d d i d % e e e c % c h e i c a
i e % e i c a i a % % % % e e d CV e a
b % i e d i d i f f e e % % e a % e (Fig e S21 a d S22, S -
% g I f a %). Tab e 1 h % e d e i e d aa e % .
N % f Tab e 1 % a % h e e i c e a e d d i f f i c e f c i e %
% % CV d a % (e % a $10^{-14} \text{ cm}^2 \text{ s}^{-1}$), % e i a %

2. The signification and units of formula symbol.

Symbol	Signification	Units
i	Reaction current	A
E	Cathode potential	V
E^0	Standard potential	V
R	Universal gas constant	$\text{J mol}^{-1} \text{K}^{-1}$
T	Testing temperature	K
n	Quantity of exchange electron	
SOC	State of charge	
$C'(R_s, t)$	Vacancies concentration on surface of spherical particles	mol cm^{-3}
$C(R_s, t)$	Li-ions concentration on surface of spherical particles	mol cm^{-3}
K_{eq}	Equilibrium constant	
K_{Re}	Reduction reaction rate constant	cm s^{-1}
K_{Ox}	Oxidation reaction rate constant	cm s^{-1}
F	Faraday constant (96487 C mol^{-1})	C mol^{-1}
A	Specific interfacial surface area	cm^2
K^0	Interfacial rate constant	cm s^{-1}
α	Symmetry factor	
D_{Li}	Li-ion diffusion coefficient	$\text{cm}^2 \text{s}^{-1}$

c e e %a %a e (Fig e 3a), hich c d b e e ai ed b %e c ic c ce %a% a i a%. He ei , e ca e %a%e diff i c ef cie %f LiFePO₄ i highe %a 10⁻¹⁴ c² s⁻¹. I addi% , %e Li-i diff i c ef cie %f LiFePO₄ ee a %e a e b %i a e a d ga ic eec% %i diffe e %e a %e . B c %a %e i % facia a % c % %f LiFePO₄ h age diffe e ce i a e a d ga iceec% % . The i % facia a % c % % fa e eec% %i e de highe %a %a% ga iceec% % de %e a e % e a % e , a d %e i % facia a % c % %f LiFePO₄ i a i % e a % e , hich age e i % %e e a % ef a ce f LiFePO₄ a % % e a % e .^[22] Acc di g % %e i a % da% (Tab e 1) a d e i^[15] e ded ce %a%e i % facia a % c % % h d be %e a % de % i i g fac% , hich e ai %e e ce % a % ef a ce i a e eec% %f LiFePO₄ . We a %d %e di cha ge ce (Fig e S23, S % g I f a %) , %e e e a % c ef cie %a e e a %e a e a %e i cha ge ce (Tab e 1).

Th gh i ea % g %e K⁰ e % e a % e , hich d c i cide %e i % face i e % A he i e a % (K⁰ = A-E_a/RT, K⁰: i % facia a % c % % E_a: ac % a % e e g ; A: e-e e %a fac% ; R: a ga c % % T: %e - d a ic % e a % e) (Fig e S24 a d S25, S % g I f a %) , e ca ge %E_a a d A b %i cha ge a d di cha ge ce e . I % e % g , e f d %a%e ac % a % e e gie



F 4. a,b) The interfacial reaction profiles for Li-ions transport across the FePO₄/water interface and FePO₄/EC interface in the discharge process.

i a e eec% % a e i i a b %a i %e highe %a %e i ga ic (E_a(H₂O) = 38.66 ± 2 J⁻¹; E_a' (ga ic) = 33.54 ± 2 J⁻¹, d i g cha ge ce a h i Fig e S24, S % g I f a %) , %e a % e de a ge i % facia a % c % %i a e eec% % ca be a % b %d % %e a ge e-e e %a fac% (A_{H2O} = 1.97 * e⁻⁸; A₀ = 2.96 * e⁻⁹). Acc di g % %e A he i e a % , e ca ge %E_a (E_a = 39.74 ± 1 J⁻¹; E_a' = 37.50 ± 1 J⁻¹) a d A (A_{H2O} = 1.77 * e⁻⁸; A₀ = 2.95 * e⁻⁹) i %e di cha ge ce . T e ai %e ab e e % , e de ic %e i % facia eac% a d Li-i diff i e f LiFePO₄ i %e cha ge a d di cha ge ce , a h i Fig e S26 f %e S % g I f a % a d **Figure 4**, e ec%e . Ta i g %e di cha ge ce , f e a e , %e i % facia eac% c %i %e e % : Li-i f eec% % % %e face f LiFePO₄ % gh a de a % ce , %e a % ched face Li-i %a %ac %e face % %e b face, a d %e Li-i diff e i %e b FePO₄. The % % i ai de % i ed b %e de a % ce , i c di g %e i g a % a d %e e e g c % % hich a de % i e %e e-e e %a fac% A. The ef % % a e ai e ec %d b ac % a % e e g (E_a) a d diff i c ef cie % (D_{Li}), e ec%e . A %e b LiFePO₄ i i a %d f %e eec% % , %e D_{Li} h d be %e a e i b %a e a d ga iceec% % , a c ed b %e CV %d da% . Acc di g % e i di g ,^[15] %e i a a a a % ec e a % ched a % %e % ca %d c e f %e face FeO₆ ched i a e eec% % (Fig e 4a), %e eadi g % % ge bi di g f %e face Li. S %e E_a f %e face Li-i %a %ac %e face % %e b face i a e eec% % i a i %e highe %a %a% i ga iceec% % , hich e ai %a%e age a e f E_a i a e eec% % b %i ed f %e CV % g . B c %a %

4.3.1. BV Model

As for the process of discharge at the cathode, $\text{LiFePO}_4 \rightarrow \text{FePO}_4^- + \text{Li}^+$, almost all the previous literatures use the porous-electrode cell model that accord with the BV equation to describe it. In order to simplify the model we assumed that the reaction just takes place at the solid and liquid phase process and does not generate gas. The active materials in the positive electrode can be modeled as spheres of radius R_s which is kept constant in the whole process. Besides, the heat coupled with the reaction can be ignored and Li-ion diffusion coefficient has no relation with the SOC. The formula symbol appeared in the BV model and the MHC theory model was depicted in Table S1 of the Supporting Information.

So Li-ion in the solid phase is assumed to move via the Fick's diffusion law, as it is shown in Equation (7)

$$\frac{\partial C(x,t)}{\partial t} = \frac{D_{\text{Li}}}{x^2} \frac{\partial}{\partial x} \left(x^2 \frac{\partial C(x,t)}{\partial x} \right) \quad (7)$$

And the boundary condition at the $x = R_s$ can be expressed as

$$\frac{i}{FA} = D_{\text{Li}} \left[\frac{\partial C(x,t)}{\partial x} \right]_{x=R_s} = k_f(t)C(R_s,t) - k_b(t)C'(R_s,t)^\alpha C^{s(1-\alpha)} \quad (8)$$

$$k_b(t) = k^0 \exp \left\{ -\alpha \frac{F}{RT} [E(t) - E^0] \right\} \quad (9)$$

$$k_f(t) = k^0 \exp \left\{ (1-\alpha) \frac{F}{RT} [E(t) - E^0] \right\} \quad (10)$$

Since the flux in the center of particle equals to zero, the other boundary condition is

$$D_{\text{Li}} \left[\frac{\partial C(x,t)}{\partial x} \right]_{x=0} = 0 \quad (11)$$

With different electrochemical parameters such as k^0 , α , D_{Li} , and the boundary conditions we can use mathematical methods to solve the partial differential equation and to recreate a CV curve.

Rigorously, the measured current in the CV test is associated with four parts: Li-ions diffusion in the LiFePO_4 cathode, Li-ions transport across the cathode/electrolyte interface, Li-ions diffusion in the bulk electrolyte, and the IR drop. In our experiments, the last two factors are not the rate-limiting step. At the same time, the Li-ions diffusions inside or outside the LiFePO_4 nanoparticle should be independent from the electrolytes used, either aqueous or nonaqueous.

4.3.2. MHC Theory Model

Compared with traditional BV model, the biggest advantage of MHC theory model is that it can characterize the whole electrochemical kinetics process in the angle of microscopic. The physical mass transfer process and the boundary condition of the MHC model were identical with the BV model. We would not elaborate further here. As well as for the process of discharge at the LiFePO_4 similar single particle thin film electrode $\text{LiFePO}_4 \rightarrow \text{FePO}_4^- + \text{Li}^+$ the current of the reaction can be depicted by the equation (Equation (12))

$$i = FA \left[-K_{\text{red}}^{\text{MHC}} \tau_{\text{red}} + K_{\text{ox}}^{\text{MHC}} \tau_{\text{ox}} \right] \quad (12)$$

According to Marcus-Hush charge transfer equation, the reduction rate constant and the oxidation rate constant are

$$K_{\text{red}}^{\text{MHC}} = K_0^{\text{MHC}} \exp \left(-\frac{\theta}{2} \right) \frac{l(\delta, \theta)}{l(\delta, 0)} \quad (13)$$

$$K_{\text{ox}}^{\text{MHC}} = K_0 \exp \left(+\frac{\theta}{2} \right) \frac{l(\delta, \theta)}{l(\delta, 0)} \quad (14)$$

The meaning of θ , δ , and $l(\delta, \theta)$ is

$$\theta = \frac{F}{RT} (E(t) - E_f^0) \quad (15)$$

$$\delta = \frac{F}{RT} \lambda \quad (16)$$

$$l(\delta, \theta) = \int_{-\infty}^{\infty} \frac{\exp \left(\frac{-(\epsilon - \theta)^2}{4\delta} \right)}{2 \cosh \left(\frac{\epsilon}{2} \right)} d\epsilon \quad (17)$$

With different electrochemical parameters and the boundary conditions we can use mathematical methods to solve the partial differential equation and to recreate a CV curve. We explore the effects of all parameters on the shape of the fitted curve and found that only $K_{\text{red}}^{\text{MHC}}$ can change the slope of the rising edge of the CV curves.

4.3.3. SP-Model

The physical mass transfer process and the boundary condition of SP-model were identical with the BV model. We would not elaborate further here. Careful analysis the curve drawn by the Nernst equation and discharge curve of LiFePO_4 diagram, such as in Figure S15a of the Supporting Information, we can find that the two were not consistent. Due to the kind of single particle experiment under the condition of Li-ions diffusion in the solution very fast, we temporarily do not consider Li-ions concentration in solution phase and just consider the Li-ions concentration in solid phase. For most materials such as LiCoO_2 or ternary materials, the shape of potential versus SOC is like the red line in Figure S15a of the Supporting Information. The line can be calculated from Nernst equation, i.e.,

$$E = E^0 + \frac{RT}{nF} \ln \frac{(1-\text{SOC})}{\text{SOC}} = E^0 + \frac{RT}{nF} \ln \frac{C(R_s, t)}{C'(R_s, t)} \quad (18)$$

The formula symbol appeared in the SP-model and its signification and units will be depicted in 2.

The equilibrium constant, i.e., ration of concentration of Li-ions and hole at any given potential E can be calculated from Equation (19). The equilibrium constant can also be represented by the ratio of oxidation and reduction reaction rate constant

$$K_{\text{eq}} = \frac{C(R_s, t)}{C'(R_s, t)} = \frac{K_{\text{ox}}}{K_{\text{re}}} = e^{\frac{nF}{RT}(E-E^0)} \quad (19)$$

We cannot obtain the individual oxidation and reduction rate constant from this equation. We need another hypothesis that is the relationship between active energy and over potential. We got next equation

$$\frac{K_{\text{ox}}}{K_{\text{re}}} = \frac{K^0 e^{\frac{(1-\alpha)nF}{RT}(E-E^0)}}{K^0 e^{\frac{\alpha nF}{RT}(E-E^0)}}$$

$$K_{\text{Ox}} = K^0 e^{\frac{(1-\alpha)nF}{RT}(E-E^0)} \quad (21)$$

$$K_{\text{Re}} = K^0 e^{\frac{\alpha nF}{RT}(E-E^0)} \quad (22)$$

For LiFePO₄ Equations (21) and (22) of oxidation and reduction reaction rate constant are not available. However, the next expression is still true

$$K_{\text{eq}} = \frac{K_{\text{Ox}}}{K_{\text{Re}}} = \frac{C(R_s, t)}{C'(R_s, t)} = \frac{(1-\text{SOC})}{\text{SOC}} \quad (23)$$

For the sake of calculating more conveniently, based on the discharge curve tested in different electrolyte at different temperature (the discharge curve tested at 0, 25, 50 °C in both aqueous and nonaqueous were shown in Figure 2c and Figures S19 and S20, Supporting Information), though a simple conversion we can get the relationship between K_{eq} and the potential in different electrolyte at different conditions (the discharge curve tested at 25 °C in both aqueous and nonaqueous after conversion were shown in Figure S16, Supporting Information). Finally, we submit the obtained relationship $K_{\text{eq}} = f(E)$ into Formula (24) and can get the reaction current as

$$i = FAK^0 [C(R_s, t)10^{(1-\alpha)\log_{10} f(E)} - C'(R_s, t)10^{-\alpha\log_{10} f(E)}] \quad (24)$$

Use these relationships and formulas we can simulate the CV curves tested in different condition.

n h m n

Supporting Information is available from the Wiley Online Library or from the author.

A n mn

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